available at www.sciencedirect.com

journal homepage: www.elsevier.com/locate/chnjc

Review

Artificial bioconversion of carbon dioxide

Ting-Ting Zhao ^{a,b}, Guang-Hui Feng ^{a,b}, Wei Chen ^{b,*}, Yan-Fang Song ^b, Xiao Dong ^b,
Gui-Hua Li ^b, Hai-Jiao Zhang ^a, Wei Wei ^{b,c,#}

^a School of Environmental and Chemical Engineering, Shanghai University, Shanghai 200444, China

^b CAS Key Laboratory of Low-carbon Conversion Science and Engineering, Shanghai Advanced Research Institute, Chinese Academy of Sciences, Shanghai 201210, China

^c School of Physical Science and Technology, ShanghaiTech University, Shanghai 201210, China

ARTICLE INFO

Article history:

Received 23 March 2019

Accepted 11 May 2019

Published 5 October 2019

Keywords:

Carbon dioxide

Artificial bioconversion

Solar energy

Carbon fixation

Chemical compound

ABSTRACT

CO₂ is not only the most important greenhouse gas but also an important resource of elemental carbon and oxygen. From the perspective of resource and energy strategy, the conversion of CO₂ to chemicals driven by renewable energy is of significance, since it can not only reduce carbon emission by the utilization of CO₂ as feedstock but also store low-grade renewable energy as high energy density chemical energy. Although studies on photoelectrocatalytic reduction of CO₂ using renewable energy are increasing, artificial bioconversion of CO₂ as an important novel pathway to synthesize chemicals has attracted more and more attention. By simulating the natural photosynthesis process of plants and microorganisms, the artificial bioconversion of CO₂ can efficiently synthesize chemicals via a designed and constructed artificial photosynthesis system. This review focuses on the recent advancements in artificial bioreduction of CO₂, including the key techniques, and artificial biosynthesis of compounds with different carbon numbers. On the basis of the aforementioned discussions, we present the prospects for further development of artificial bioconversion of CO₂ to chemicals.

© 2019, Dalian Institute of Chemical Physics, Chinese Academy of Sciences.

Published by Elsevier B.V. All rights reserved.

1. Introduction

In 2017, the total world energy consumption was 13.5 billion tons (oil equivalent), of which 87.7% was sourced from fossil fuels [1]. With the growth in the world population and rapid industrialization of developing countries, the global energy consumption will continue to increase. A large consumption of fossil fuels leads to a rapid increase in the CO₂ concentration in the atmosphere, causing serious environmental

problems [2]. For sustainable development of human society, there is an urgent need to develop new green technologies to realize the conversion and utilization of CO₂ resources [3,4]. Although studies on photoelectrocatalysis reduction of CO₂ by using renewable energy are increasing, artificial bioconversion of CO₂ has attracted more and more attention as an important novel pathway of synthesizing chemicals.

CO₂ is an important substantive source for the photosynthesis of plants and microbes on the earth. Organisms absorb CO₂

* Corresponding author. Tel: +86-21-20350954; Fax: +86-21-20350867; E-mail: chenw@sari.ac.cn

Corresponding author. Tel: +86-21-20608005; Fax: +86-21-20350867; E-mail: weiwei@sari.ac.cn

This work was supported by the National Natural Science Foundation of China (91745114, 21802160), the National Key R&D Program of China (2016YFA0202800), Shanghai Sailing Program (18YF1425700), and Shanghai Advanced Research Institute Innovation Research Program (Y756812ZZ1(172002), Y756803ZZ1(171003)). Wei Chen also acknowledges the support from the Hundred Talents Program of the Chinese Academy of Sciences.

DOI: S1872-2067(19)63408-X | http://www.sciencedirect.com/science/journal/18722067 | Chin. J. Catal., Vol. 40, No. 10, October 2019

from the air and synthesize nutrients with the help of solar energy. However, biological utilization of CO₂ is of low efficiency and it is difficult to continuously convert CO₂ into synthetic fuels and chemicals on a large scale [5]. In recent years, researchers have made use of microorganisms and enzymes to form biological hybrid systems to absorb CO₂, and have used renewable electrical energy and solar energy to produce biochemicals and biofuels. In addition, the photosynthetic autotrophic microbes (cyanobacteria or microalgae) that possess the ability to immobilize CO₂ were modified to obtain efficient carbon sequestration organisms through genetic engineering in order to produce high-value target chemicals [6,7].

In general, thermocatalytic conversion of CO₂, i.e., CO₂ hydrogenation, occurs under harsh reaction conditions such as high temperatures and high pressures, which require large amounts of energy to realize [8]. The source of the reactant hydrogen is also an obstacle for thermocatalytic CO₂ hydrogenation. The biggest advantages of CO₂ hydrogenation are the relatively satisfactory CO₂ conversion rate and the yield of the product methanol. Different from the thermocatalytic conversion of CO₂, CO₂ photoreduction, electroreduction, and bioreduction can occur under mild conditions even at ambient temperature and pressure when driven by renewable energy such as solar light and renewable electricity. The efficiencies of the photocatalytic and electrocatalytic reductions of CO₂ are relatively higher than that of CO₂ bioconversion [9–15], as shown in Table 1. The state-of-the-art biological hybrid system Co-P[CoPi] *R. eutropha* exhibited the energy efficiency of 9.7% [9]. More complicated and valuable compounds can be produced during CO₂ bioconversion. Moreover, CO₂ artificial bioconversion, which integrates the advantages of photo/electrocatalysis and CO₂ bioreduction, shows promise.

Until now, various chemicals have been synthesized by the bioconversion of CO₂. This review summarizes the key techniques for CO₂ artificial bioconversion and their basic principles, characteristics, etc. Furthermore, the typical chemicals obtained by the aforementioned techniques are classified by their carbon number and exemplified. The prospects for further

development of artificial bioconversion of CO₂ to chemicals are also presented.

2. Key techniques of CO₂ artificial bioconversion

Artificial bioconversion of CO₂ is an important complement to the CO₂ conversion aided by renewable energy, besides the CO₂ electrocatalytic, photocatalytic, and photoelectrocatalysis conversions. The highlight of CO₂ artificial bioconversion is the combination of active biofeatures and physicochemical catalytic sites. Until now, the key techniques of CO₂ artificial bioconversion mainly include microbial electrosynthesis (MES), photosynthetic biohybrid systems, PSII (photosystem II) hybrid system, and metabolic engineering.

2.1. Microbial electrosynthesis

MES is based on the use of specific microorganisms as biocatalysts in microbial bioelectrochemical systems, with electricity as the source of energy. Reducing CO₂ to multi-carbon compounds through biological reactions is one of the most promising emerging technologies (Fig. 1 shows a typical MES system for CO₂ reduction) [16–19]. Enzymes are also suitable for the biosynthetic processes in MES (also described in this work) because they share the same function as microorganisms of synthesizing a single product, with a selectivity of 100% [20]. MES needs electrical energy to provide electrons and to control the electrode potential for CO₂ reduction, while the external power supply increases the cost of the whole synthesis process. Previous studies have shown that the overall cost of MES should be further reduced to achieve economic competitiveness and environmental sustainability [21,22]. Fortunately, the electrical energy has a wide range of sources and can be regenerated from sustainable forms such as solar, wind, nuclear, and water power, which make MES a green and sustainable CO₂ conversion technique [23–26]. However, the widespread use of these renewable energies is limited by their instability and intermittency, which renders the storage and utilization of renewable electricity difficult [27]. The conversion of CO₂ into chemicals and biofuels in MES is still in its infancy, and there are many technical and economic challenges that need to be addressed, such as the high power demand and the low

Table 1

Energy efficiency comparisons of the various technologies for CO₂ conversion.

Technology	System/Material	Product	Energy efficiency (%)	Ref.
Artificial bioconversion	Co-P[CoPi] <i>R. eutropha</i>	Biomass	9.7	[9]
		Poly(3-hydroxy butyrate)	7.6	
		C ₃ -C ₅ alcohols	7.1	
	CoPi <i>R. eutropha</i> NiMoZn/stainless-steel	Biomass	3.2	[10]
		Isopropanol	0.7	
Photocatalysis	GaInP/GaInAs/Ge photovoltaics	CO	13.4	[11]
	Series-connected perovskite cells	CO	6.5	[12]
Electrocatalysis	Ag ₂ S in ionic liquids	CH ₄ , CO	58.5	[13]
	Au nanoneedle NiCoFeP	CO	64.0	[14]
	SnO ₂ quantum wires	HCOO ⁻	52.7	[15]

Fig. 1. Scheme of a microbial electrosynthesis system [18].

productivity. Despite these challenges, the use of electricity or solar energy as the driving force of biological carbon sequestration has two benefits: first, it can improve the efficiency of biological carbon sequestration; second, solar energy can be stored sustainably in the chemical bonds of multi-carbon products [28].

The low efficiency of biocathodes seriously hinders the MES productivity, which is mainly because of the barriers of charge extraction and injection between the biological and abiotic interfaces of the biological and electronic systems, namely the low charge transfer efficiency across the biological-abiotic interfaces, presenting an important obstacle to the efficient integration of biological and electronic systems [29]. Therefore, the key to MES optimization is to enhance the electron exchange on the cathode surface. At present, there has been a great improvement in understanding how organisms transfer electrons to electrodes, but the mechanism of electron transfer from the electrode to the microbe is still unclear. Although the improved method for biomaterials may still be experiential to a large extent, it works. At present, low-cost MES cathode materials mainly include carbon cloth, carbon paper, carbon felt, stone mill rod, glass carbon rod, and other carbon materials [30–35]. However, when a conventional electrode material is used as the biological electrode, its poor compatibility with organisms and small specific surface area are not conducive to full attachment of microorganisms and charge transfer at a high efficiency. The three-dimensional nanostructure of the highly conductive nano-reticulated glass carbon (Nano Web-RVC) electrode enhances the current density of the MES system. Its layered pores in this unique electrode structure can support a large number of microorganisms and facilitate mass transfer [36]. In addition, the material is inexpensive and easy to be popularized on a large scale. Besides, a novel conductive microbial nanowire electrode can promote the long-distance transfer of extracellular electrons and increase the conductivity [37]. The conductive filaments can also be used to cultivate microbial strains with a better electrical conductivity. Therefore, study of the interaction between bacteria and nanostructures may improve the MES systems that are dependent on extracellular electron exchange to obtain controllable interfaces between biological and abiotic components [38]. Silicon nanowire arrays ensure a good interaction between nanostructures and cell units. Silicon nanowire arrays with a high specific surface area can promote the reduction of CO_2 and improve the performances of typical low-density microbial catalysts [38,39]. Surface modification of carbon materials by physical or chemical methods can also improve the performances of electrode materials [30].

In addition to direct utilization of external power, it is also possible to use the electricity generated via reverse electrodialysis from the green and sustainable salinity gradient energy as the driving force of MES to achieve efficient CO_2 bioconversion [40,41]. It has been reported that a microbial reverse-electrodialysis electrolysis cell (MREC) can help realize this technology [42]. The salinity gradient is rich in energy and exists in various environments, such as seawater and river water; high/low salinity is produced by wastewater treatment. Therefore, the system can not only make use of wastewater to

generate electricity, but also purify wastewater. However, this kind of energy has not yet been effectively captured and stored, and access to this energy requires the development of an effective energy conversion technology. This new technology can produce biofuels and treat wastewater at the same time, which reduces the sewage treatment cost, increases power generation, and also provides a potential technology platform for the collection and storage of salinity gradient energy and CO_2 emission reduction.

2.2. Photosynthetic biohybrid systems (PBSs)

A PBS is a novel photo-driven device composed of bacteria or enzymes that are immobilized on inorganic semiconductor photocatalysts; it combines high-efficiency inorganic photocatalysts with enzyme catalysts or cellular organisms [20]. The efficiency of selective fixation of CO_2 is close to or higher than that of natural photosynthesis or chemical catalysis [24,43]. Although the light absorption efficiency of inorganic semiconductors is higher than that of natural photosynthesis, these artificial photocatalysts do not display the high selectivity, low energy consumption, self-replicating, and self-healing properties of natural catalysts. In addition, the incredible biosynthetic ability can be used to not only reduce CO_2 but also obtain the target products in a cost-effective and highly selective manner under mild conditions and to synthesize long-chain hydrocarbons on a large scale.

The possible structure of PBSs is shown in Fig. 2. A PBS utilizes the light-capturing performance of semiconductors to obtain photogenerated electron-hole pairs that decompose water into hydrogen and oxygen and then convert CO_2 into value-added chemicals via the metabolic pathway in organisms to obtain organic acids and methane [44–47]. It can also be considered as a MES reactor that is powered by solar energy, or a modified MES electrode that directly captures light energy, thus effectively functioning as an artificial photosynthesis device that exhibits a higher solar energy efficiency than natural photosynthesis [48]. Some of these systems have been demonstrated in recent studies, and many methods have been provided to realize this concept. The high product selectivity also proves the effectiveness of the combination of biological CO_2 reduction and inorganic light capture technology. Silicon nanowires, $n\text{-TiO}_2$ nanowire/FTO, $n^+/p\text{-Si}$, $p\text{-InP}$, metal sulfide/oxide nanoparticles (mainly CdS and TiO_2), etc. have been reported as light-capturing devices for inorganic biological

Fig. 2. Scheme of a photosynthetic biohybrid system [20].

hybrid systems.

PBSs are still in the early stage of development. In spite of the possibility of achieving higher solar conversion efficiencies (10% to 20%), several technical parameters still need to be improved, and there is still a long way to go before they can be widely implemented [49]. One of the main challenges is the selection of compatible optical capturing systems and efficient biological carbon sequestration units, as well as the seamless integration of biological and non-biological components. In other words, it is still a challenge to overcome the charge transfer barrier at the cross-biological and abiotic interfaces (mentioned in section 2.1). At this point, semiconductor electrodes with high specific surface areas, such as semiconductor silicon nanowire arrays, are ideal for obtaining high current densities under illumination [30]. In the future, new electrode materials with good electron active surfaces, low overpotentials, high specific surface areas, good biocompatibilities, and high electron transfer efficiencies need to be developed. The cost of the material needs to be considered as well. At present, electrode materials displaying the performance described above are scarce, therefore, it is imperative to reform and develop new electrode materials.

2.3. PSII composite system

The PSII composite system is one of the most recently proposed artificial photochemical systems that consists of natural PSII and artificial photocatalysts. Alternatively, PSII is used to modify the MES electrode to facilitate the reduction of CO₂ in an artificial photochemical system [50,112]. Compared with that of PBSs, the biological enzyme of the PSII complex system is PSII. The PSII complex system can reproduce the biological characteristics of PSII, such as the excellent light collection ability. PSII can efficiently capture the energy of the visible solar spectrum across all wavelengths, which can be used to drive the decomposition of water to obtain hydrogen equivalent, which is also a unique advantage, compared with an inorganic photocatalyst.

PSII is a photoactive complex located on thylakoid membrane (TK) in green plants, cyanobacteria, and microalgae [51,52]. It can convert solar energy into chemical fuels and provide the materials and energy for almost all living creatures, including humans. The water-cleavage reaction is the origin of the whole photosynthesis process. The information found regarding the structural determination of PSII has a significant impact on the design of artificial catalytic systems that utilize solar energy to release hydrogen equivalent from water. Mn₄Ca clusters in PSII are the only biocatalysts in nature that can use solar energy to oxidize water efficiently and safely and release oxygen, “high energy” electrons, and protons. It can be used in visible-light-driven water photolysis. The resulting hydrogen can be used directly as an energy source or used in photosynthesis to reduce CO₂ into other fuels, such as methane. It is considered to be the best hope of developing new technologies that convert solar radiation into usable energy sources [4,50].

Some studies on visible-light-driven hydrogen production of PSII have been reported. Further, artificial photochemical sys-

tems have been established to simulate the hydrogen production of the active centers in PSII. These works are of significance in further obtaining or optimizing the PSII composite system to reduce CO₂ [50,53–55]. Fig. 3 illustrates the charge separation in PSII, the direction of electron flow, and the water cracking reaction and the final CO₂ reduction reaction. In PSII, the light energy captured by the light-harvesting complex is rapidly funneled into the chlorophylls bound in D1/D2 subunits, resulting in charge separation and a series of electron transfers that lead to Q_B cofactor. The evolution of O₂ and proton (H⁺) occurs on Mn₄CaO₅ clusters due to water oxidation. CO₂ may bind to the hydrogen equivalent released from PSII and then be reduced by inorganic catalysts, enzymes, and microorganisms to formic acid, methanol, and other chemicals [42].

There has been a lot of research on photovoltaic conversion systems assembled on electrodes using PSII, and some initial progress has been made. However, studies on CO₂ reduction are still very limited. In addition, *in vitro* purified PSII will result in irreversible photodamage under illumination, which renders it highly unstable. The long-term anti-light stability of PSII on the electrode is a serious problem affecting the use of photovoltaic converters [56].

2.4. Metabolic engineering

Metabolic engineering is an applied discipline in which cellular metabolic pathways are reasonably designed according to cellular metabolic networks, and molecular biological means (such as recombinant DNA technology) are used to design and regulate the existing metabolic networks and expression regulatory networks in organisms purposefully [57–59]. In order to achieve more efficient biochemical transformations, energy transfer, and accumulation of the target products, analysis of the metabolic function of modified organisms is one of the core technologies of metabolic engineering. At present, metabolic engineering has been widely used in photosynthetic biological carbon sequestration to further optimize the resource utilization of CO₂ to biomass or other organic compounds.

Photosynthetic autotrophic microalgae with CO₂ fixation

Fig. 3. Scheme of a PSII-catalyst hybrid system for solar-powered CO₂ fixation [50].

capacity can be grown on a large scale on non-cultivated lands. Microalgae usually exhibit a higher photosynthetic efficiency than other biomass such as trees. Microalgae biotechnology, especially microalgae bioenergy, has emerged as a hot research topic at home and abroad in recent years. Sustainable energy production in the future could be achieved through a large number of photoautotrophic microorganisms [60,61]. Researchers used metabolic engineered autotrophic organisms (such as cyanobacteria) or exotic organisms (such as *Escherichia coli*; *E. coli*) to introduce reaction pathways for target chemicals into the body through metabolic engineering and eventually synthesize fuels and chemicals from CO₂ [62,63]. The relatively high yield of ethanol, which can be of the order of grams per liter, shows the potential of bio-carbon sequestration [64]. It is also possible to utilize the carbon sequestration pathway in organisms to construct an effective in vitro system that can transform CO₂ into value-added chemicals [65].

Low energy efficiency and low carbon sequestration rate are two bottlenecks of natural photosynthesis. They are also the major challenges in basic and applied research [66]. The mismatch between the light reaction and dark reaction energies is one of the key factors limiting the photosynthesis energy efficiency and carbon sequestration rate [67,68]. The synthesis of isopropanol, which consumes additional NADPH in cyanobacteria, can balance the reduction power of the biological system. Thus, the photosynthetic efficiency of cyanobacteria can be greatly increased, and the growth rate and biomass of cyanobacteria can also be significantly increased [69,70]. In addition, the carbon fixation activity of microalgae can also be enhanced by regulating the RuBisCO activator (ribulose-1,5-diphosphate carboxylase) of oil-producing microalgae, thus greatly increasing the biomass and oil yield of microalgae [71].

E. coli has emerged as one of the most important model strains for studying artificial carbon sequestration in recent years. The Calvin carbon fixation cycle was successfully constructed in *E. coli* to realize the synthesis of sugars and other biomass, which is required for the growing demand due to CO₂ [72,73]. RuBisCO, the key enzyme of photosynthetic carbon fixation in *E. coli*, will be helpful in improving the efficiency of carbon sequestration if it can be modified by mutation or other ways and lays the foundation for the increase in the grain yield [74,75].

By studying metabolic engineering, raising awareness, designing and transforming the ability of the cell to metabolize CO₂, a carbon sequestration pathway with low energy consumption and high efficiency can be obtained, and the biological carbon fixation industry will technologically progress, which is an important development in this field.

3. Artificial biosynthesis of various compounds

3.1. C₁ compounds

The most common C₁ compounds synthesized by MES are carbon monoxide, methane, formic acid, and a small amount of methanol. It is usually produced by the conversion of CO₂ from methanogenic cultures and some targeted dehydrogenase

Table 2

Reduction routes and the corresponding theoretical potentials of C₁ compounds synthesized by CO₂.

Reduction route	Theoretical potential <i>E</i> ⁰ (V vs. NHE)	Series number
CO ₂ + e ⁻ = CO ₂ ^{•-}	-1.90	(1)
CO ₂ + 2e ⁻ + 2H ⁺ = CO + H ₂ O	-0.53	(2)
CO ₂ + 2e ⁻ + 2H ⁺ = HCOOH	-0.61	(3)
CO ₂ + 4e ⁻ + 4H ⁺ = H ₂ CO + H ₂ O	-0.48	(4)
CO ₂ + 6e ⁻ + 6H ⁺ = CH ₃ OH + H ₂ O	-0.38	(5)
CO ₂ + 8e ⁻ + 8H ⁺ = CH ₄ + 2H ₂ O	-0.24	(6)

[76,77]. Equations (1)–(6) in Table 2 show the possible reduction routes and the corresponding theoretical potentials for the synthesis of C₁ compounds by CO₂ (in aqueous solutions with pH = 7) [78–81].

In most research, the formations of C₁ products are based on reductive coenzymes, such as NADH, which provide the electrons and hydrogen equivalent. In the presence of three dehydrogenases, namely, formate dehydrogenase (FDH), formaldehyde dehydrogenase (ALDH), and alcohol dehydrogenase (ADH), for every two-electron reduction step of CO₂, one NADH molecule is oxidized to NAD⁺ in a three-step cascade. However, this irreversible oxidation of NADH is expensive to realize because of the high cost of synthesis and regeneration, which limits the application of enzymes in the reduction of CO₂ [82–84]. Therefore, a proper replacement for coenzymes is quite necessary, especially direct injection of electrons into the enzyme, which has high application value [85].

The general formation mechanisms of the C₁ products of CO₂ artificial bioconversion process are first summarized. Carbon monoxide dehydrogenase (CODH) plays a key role in CO formation from CO₂, which is reduced on the nickel- and iron-containing active sites of CODH [86]. At reducing potentials, CO₂ acts as a bridging ligand between the nickel and the dangling iron atom to form a square planar arrangement around the nickel; then, a OH unit forms on the iron and CO species may be generated on the nickel sites. There are two mechanisms for methane production by microbial reduction of CO₂: (1) the H₂ produced on the cathode surface of MES is utilized by the hydrophilic methanogenic bacteria attached to the surface of the cathode to produce methane by binding with CO₂; (2) the cathode-functional microorganism can directly obtain the electron from the cathode surface to reduce CO₂ to methane [86–88]. In the presence of three dehydrogenases, including formate dehydrogenase, formaldehyde dehydrogenase, and alcohol dehydrogenase, for every two-electron reduction step of CO₂, one NADH molecule is oxidized to NAD⁺ in a three-step cascade, as shown in Fig. 4 [89].

3.1.1. Carbon monoxide

CO is the raw material of various synthetic processes and

Fig. 4. General reduction mechanisms of CO₂ artificial bioconversion process [89].

can be easily converted into liquid fuels such as methanol. Woolerton et al. [90] built a PBS that reduced CO_2 to CO under visible light irradiation. The system used TiO_2 nanoparticles modified by CODH. The researchers utilized polypyridine ruthenium, which is sensitive to visible light, to reduce the CO_2 overpotential. The principles are shown in Fig. 5A. Upon excitation with visible light, RuP injects electrons into the conduction band of TiO_2 . These electrons can then enter CODH through the D-cluster and are transferred through a second [4Fe-4S] cluster to the active site, where CO_2 is reduced to CO by enzymatic action through a two-electron reduction pathway. The measured turnover rate was around 0.14 mol CO produced (mol CODH) $^{-1}\text{s}^{-1}$. The semiconductor acts as a scaffold for enzyme and dye molecules: experiments in which TiO_2 was omitted yielded no detectable CO. Secondly, the conduction band maintains the energy of the photoinjected electrons above a minimum potential threshold, which is sufficient for CO_2 reduction by CODH. Fig. 5B presents the effect of other semiconductor materials on the production of CO in the system. It was found that the combination of a photosensitizer with ZnO was poor: only around 60% of the 56 nmol RuP added was bound to ZnO after 20 min adsorption period, compared with that of almost 100% for TiO_2 . They used *o*-phosphorylethanolamine (OPEA) to modify the surface of TiO_2 . As shown in Fig. 5C, rather than obtaining the desired effect, the modified layer decreased the rate of catalysis; this is (at least in part) due to the lower uptake of an enzyme when OPEA is added. The two-electron pathway of the highly efficient and specific CO_2 reduction model system can avoid the thermodynamic barrier involved in the single-electron activation pathway and provides a lot of information and constructive insights into solar-driven reduction of CO_2 emissions [91].

3.1.2. Methane

Methanogens can reduce CO_2 to methane with H_2 [92]. Methane is a good fuel that can be favorably separated because of its low solubility. The direct conversion of CO_2 to CH_4 by using synthetic catalysts is still a huge challenge because of its high overpotential and low CH_4/H_2 selectivity. The Faraday efficiencies of the direct electrocatalytic methanogenic conversion of two kinds of CO_2 with high activity and selectivity to CH_4 were 61% and 76%, respectively, but the overpotentials (η) required were 1.28 V and 1.52 V [93,94]. Cheng et al. [95] reported for

the first time that CO_2 can be reduced to methane by *Methanobacterium palustre* under the condition that the cathodic potential is less than 0.7 V (vs. Ag/AgCl). The continuous yield of methane is 200 mmol- CH_4 d $^{-1}$ m $^{-2}$, and the electron capture efficiency 96%.

Nichols et al. [96] used *Methanosarcina barkeri* (*M. barkeri*) biocatalyst to reduce CO_2 to CH_4 . Fig. 6A shows a general schematic of the gastight, two-compartment electrochemical cell that was specially designed for batch-mode electrolysis and subsequent headspace analysis by gas chromatography. The cell employs platinum or an earth-abundant substitute, such as α -NiS, as the biocompatible hydrogen evolution reaction (HER) electrocatalyst and *M. barkeri* as the biocatalyst for CO_2 fixation. In Fig. 6B, the variation in the applied current from 1 mA to 7.5 mA shows that the CH_4 generation is proportional to the applied current, suggesting that the system is operating in a hydrogen-limited regime. When the applied current is 2.5 mA, the system displays high Faradaic efficiencies (of up to 86%) and a low overpotential (η = 360 mV). A slight decrease in the Faradaic efficiency is observed at higher current densities. The researchers then replaced the expensive platinum with nano- α -NiS, the electrocatalytic performance of which is presented in Fig. 6C and Fig. 6D. When the current is increased to 7.5 mA, the results obtained from experiments using α -NiS/C are virtually indistinguishable from those obtained with platinum in terms of the daily and cumulative amounts of methane generated; 4.24 mmol of CH_4 is produced over 7 days, with an average Faradaic efficiency of 74%. In addition, photoactive cathodes were prepared by sputtering a thin layer of nickel-molybdenum alloy atop TiO_2 -passivated n-/p-Si. At 2.5 mA and only 175 mV overpotential, biological galvanostatic electrolysis generated 0.692 mmol CH_4 , with the Faradaic efficiency being 82%, which allowed more methane to be produced for a certain amount of electricity. On the other hand, for the combination of n- TiO_2 photoanode and p-InP photocathode, CO_2 can be converted into CH_4 without being driven by light.

3.1.3. Formic acid

Song et al. [97] reported that two acetogenic bacteria, *Moorella heatacetica* (*Mt*) and *Foricoaceticum* (*Cf*), can effectively convert CO_2 to formic acid below 0.58 V, with the current efficiencies being 80% and 100%, respectively. Lee et al. [98] reported the highly selective reduction of CO_2 to formate on a

Fig. 5. (A) Cartoon representation of CO_2 reduction at an enzyme-modified metal oxide nanoparticle sensitized with a ruthenium dye; (B) CO production for 5 mL suspensions of various semiconductors modified with *Ch* CODH I (2.56 nmol) and RuP (56 nmol); (C) Effect of OPEA modification of TiO_2 on CO production [90].

Fig. 6. (A) Electrochemical reduction of carbon dioxide to methane on a hybrid platinum/*M. barkeri* platform; (B) Cumulative methane generation and the associated average Faradaic efficiencies obtained at various currents; (C) Polarization curve; (D) Methane generation and the associated average Faradaic efficiency [96].

tightly integrated bioelectrode. They used the multifunctional polydopamine (PDA) membrane with biocompatibility and good charge transferability as the substrate for the immobilized enzymes NADH (C, NADH) and FDH (E, FDH), which acted as the electron mediator and reaction catalyst, respectively [99], as shown in Fig. 7A. This bio-hybrid system with nanometer thickness not only promoted electron transfer but also kept the enzyme stable on the electrode for a long time (for about two weeks) [100]. In Fig. 7B, the much lower capacitive current of the EC-PDA layer in comparison to that of PDA indicated that a denser and/or thinner film was formed when EC was incorporated into the PDA film [99,101]. In addition, a sustainable energy conversion system composed of nano-porous COPI/BiVO₄ photoanode and EC-PDA biocathode without an external bias was designed [102,103]. Fig. 7C shows

Fig. 7. (A) Schematic illustration of the 3D structure and the proposed formation mechanism of EC-PDA thin film-coated biocathode; (B) Cyclic voltammograms of PDA and EC-PDA coated GCE; (C) Linear sweep voltammogram; (D) Photocatalytic formate formation from CO₂ gas as a function of irradiation time [98].

the *I-V* curves of the EC-PDA double electrode structure under light and dark conditions, which can be used to estimate the difference in the open-circuit voltage between the light and dark conditions as 400 mV. The open-circuit voltage increased by 110 mV and the short-circuit current doubled, indicating that CoPi is a good OER catalyst that can effectively reduce the kinetic overpotential of the photoanode. For long-term stability tests, the current density was monitored for 24 h at a constant voltage of 0 V (vs. CoPi/BiVO₄ photoanode), and the result is displayed in Fig. 7D. The chronoamperometric current was low, but stable at $-0.1 \mu\text{A cm}^{-2}$, and was believed to result from the fast kinetics at the cathode and dissolution of CO₂ into the aqueous solution, as revealed in the inset of Fig. 7D. The amount of formate produced increased linearly with the reaction time, and $15 \mu\text{mol L}^{-1}$ formic acid was produced after 24 h. HPLC analysis result clearly reveals that formate is the only product of light-driven CO₂ reduction by EC-PDA biocathode, with the Faradaic efficiency being almost perfect at 100%.

Amao et al. [104] studied the preparation of TK assembled on TiO₂ thin film electrode and its photocurrent conversion function. By using PSII as the photocatalytic material for oxygen production, a composite electrode with PSII function was prepared. Oxygen evolution with PSII in TK/TiO₂ occurs under visible-light irradiation. Electron transfers from TK to the conduction band of TiO₂, and then from TK/TiO₂ to the co-immobilized FDH-CH₃V(CH₂)₉COOH cathode via the external circuit. CO₂ is then reduced to formic acid by FDH at the cathode. Formic acid and oxygen are formed in the stoichiometric ratio of 2:1.

3.1.4. Methanol

Formic acid is the main product in most studies, with trace amounts of formaldehyde or methanol. One of the reasons is the strong equilibrium of formaldehyde on methanol hydrate [105,106]. Scientists often use the coenzyme NADH to produce methanol. However, there have been few attempts at reducing CO₂ to methanol and few reports on methanol products. Yadav et al. [107] reported selective methanol production for the first time by visible-light-driven CO₂ reduction in PBSs. In this study, IP (isatin-porphyrin) chromophore covalently binds to chemically converted graphene (CCG) to form the visible light active photocatalyst CCG-IP, as shown in Fig. 8A [108]. CCG acts as an electron storage layer to transport multiple electrons. CCG-IP exhibits efficient visible light capturing capability, providing energy for efficient regeneration of NADH, which is an essential condition for methanol generation from CO₂ [109]. Fig. 8B shows that CCG-IP linearly accumulates 38.99% of NADH within 60 min. On the other hand, CCGMAQSP (chemically converted graphene coupled multi-anthraquinone-substituted porphyrin) photocatalyst and IP chromophore regenerated 28.46% and 7.03% of NADH within the same time frame, respectively. However, CCG failed to regenerate any NADH. Methanol of concentration $11.21 \mu\text{mol L}^{-1}$ was obtained on exposure to visible light over the subsequent 60 min when CCG-IP was used as the photocatalyst. On the other hand, only $5.62 \mu\text{mol L}^{-1}$ of methanol was obtained upon the use of CCGMAQSP as the photocatalyst. The experiment with IP

Fig. 8. (A) 3D structure of CCG-IP photocatalyst, along with the detailed chemical structure of IP chromophore; (B) Photocatalytic 1,4-NADH regeneration activity; (C) Production of methanol; (D) Photocurrent-time (I-T) profiles of FTO/IP and FTO/CCG-IP electrodes under simulated solar light illumination [107].

chromophore afforded a trace amount of methanol, which could not be quantified, while CCG failed to produce any methanol, as observed in Fig. 8C. The result of transient photocurrent study in Fig. 8D shows that the prompt photocurrent response of CCG-IP corresponds well with the ON/OFF cycles of the simulated sunlight irradiation. It indicates electron transfer from IP to CCG upon irradiation, which leads to regeneration of the enzymatically active 1,4-NADH and subsequent methanol formation [108].

Schlager et al. [89] reported a method of direct CO₂ reduction by MES that involves injecting electrons directly into the electrode without the need for the expensive coenzyme NADH. FDH, ALDH, and ADH are immobilized in matrices to ensure high stability of the enzyme and high activity and reusability of the biocatalysts, as shown in Fig. 9A [110]. Fig. 9B indicates that a methanol peak appears at a residence time of 1.85 min after electrolysis for 4 h. Around 0.15 ppm of methanol is detected in the electrolysis experiment at a constant potential of 1.2 V (vs.

Ag/AgCl), which corresponds to a Faradaic efficiency of around 10%. For the samples not subjected to electrolysis, where the enzyme electrode is stored only in a saturated solution of CO₂ or H₂, no methanol peak can be observed. This method provides the possibility of selective reduction of CO₂ emission under mild operating conditions.

Lian et al. [111] prepared a kind of photoelectric catalytic cell with self-reducible CO₂ by using PSII modified photoanode. The system uses copper foam as the photoanode and p-silicon nanowires (Si-NW) as the photocathode. Under sunlight irradiation, PSII decomposes water to generate hydrogen and electrons. Electrons transfer rapidly from PSII to the Cu foam, and then, the Si-NW capture the electrons in an external circuit at 0.5 V bias. Its appropriate conductive band potential (of 0.6 eV) makes it easier to reduce CO₂ to methanol at the photocathode.

3.2. C₂ compounds

Generally, the generation mechanisms of C₂ products from CO₂ artificial bioconversion are more complicated, and involve C–C coupling in biological carbon sequestrations. There are carbon sequestration pathways that can directly fix CO₂. They are Calvin cycle, (CBB), reductive tricarboxylic acid cycle (rTCA), *Wood-Ljungdahl* pathway (W-L), and dicarboxylate/4-hydroxybutyrate cycle. The first two pathways are aerobic pathways, whereas the latter two are anaerobic pathways. The natural pathways for carbon sequestration with substrate HCO₃²⁻ are as follows: 3-hydroxypropionate cycle, 3-hydroxypropionate/4-hydroxybutyrate autotrophic pathway, and dicarboxylate/4-hydroxybutyrate cycle [112].

3.2.1. Acetic acid

Obligate anaerobic acetogen can convert H₂ and CO₂ into various fuels and chemicals such as acetic acid (CH₃COOH) through the efficient and energy-saving *Wood-Ljungdahl* pathway [100–102]. Acetic acid is the most studied C₂ product at present. *Sporomusa ovata* (*S. ovata*) is the most effective acetic acid producing strain reported so far in pure culturing [113,114].

One way to improve the reduction rate of CO₂ in the process of MES is to modify the cathode to improve the interaction between the microorganism and the electrode. Nie et al. [115] used graphite electrodes coated with porous nickel nanowires to increase the interface area and the interaction between the cathode surface and the bacterial biofilm. The biological reduction rate was increased by 2.3 times. They were given 540 mg L⁻¹ of acetic acid on day 8. A novel 3D graphene-nickel foam (G-NF) cathode has been fabricated by hydrothermal approach for the improvement of the microbially catalyzed reduction at the MES cathode. The concentration of acetic acid obtained by Song et al. [116] after 28 days of MES was 5.46 g L⁻¹. They prepared a novel 3D G-NF cathode by hydrothermal method. The hierarchical porous G-NF cathode improved bacterial colonization and the efficiency of mass, nutrient, and proton transfer owing to its 3D composition. The graphene coating considerably increased the effective surface area for microbial adhesion, as well as the electron transfer rate of the biofilm in MES. An

Fig. 9. (A) Representation of the electrochemical CO₂ reduction process using enzymes, and electrons are injected directly into the enzymes, which are immobilized in alginate silicate hybrid gel (green) on a carbon-felt working electrode; (B) Comparison of chromatograms obtained by LGC [89].

increase of 1.8 times in the volumetric acetate production rate was obtained, compared with that for untreated nickel foam.

Bian et al. [117] used porous nickel hollow fibers (Ni-PHF) coated on carbon nanotubes (CNTs) to form a new functional Ni-PHF/CNT with high biocompatibility. The material was used as the cathode to produce acetic acid through MES. Fig. 10A and Fig. 10B are the scanning electron microscope images obtained before and after the growth of *S. ovata* on Ni-PHF/CNT. The Ni-PHF surface is covered with CNTs, which further improves the surface roughness and pore density of the PHFs observed in Fig. 10A. The surface of Ni-PHF/CNT exhibits a completely bacterial structure in Fig. 10B. The 11.1 times higher CO_2 adsorption obtained in the case of the Ni-PHF/CNT cathode is possibly attributed to the deposited CNT layers, which show strong physical interactions with CO_2 molecules [118, 119]. In addition, improved CO_2 adsorption on the Ni-PHF/CNT can be due to the large surface area and geometry of the CNTs, which exhibit different regions and sites for adsorption [120]. The HERs of Ni-PHF and Ni-PHF/CNT cathodes were characterized by linear sweep voltammetry (LSV). The LSV curve of Fig. 10C shows that when the voltage is -1.0 V, Ni-PHF/CNT displays a good catalytic activity towards the HER, and the current density is 1.66 times higher than that of Ni-PHF. The Tafel slopes derived from LSV data are commonly believed to be an indication of the HER catalytic properties of electrode materials [121]. In Fig. 10C, the Ni-PHF/CNT cathode exhibits 15% lower Tafel slope (342 mV dec^{-1}) compared to that of Ni-PHF (393 mV dec^{-1}), which suggests that Ni-PHF/CNT is a better HER catalyst. Fig. 10D shows that the rate of acetic acid production is $1.85 \text{ g m}^{-2} \text{ d}^{-1}$ and the Coulomb efficiency is up to 83% when CO_2 is directly transported through the pores of Ni-PHF/CNT hollow fiber.

Liu et al. [44] developed a biologically compatible nanowire array to realize a PBS. The semiconductors silicon and TiO_2

were selected as the photocathode for hydrogen production and as the photoanode for oxygen production, and ionic conductive films were introduced between silicon nanowires and TiO_2 nanowires to realize macroscopical separation of H_2 and O_2 . In neutral pH, only solar energy was required to feed the silicon nanowire array, and the nanowire-bacteria hybrids were capable of reducing CO_2 to acetate under continuous sparging with an overpotential less than 200 mV at 0 V vs. reversible hydrogen electrode (RHE). Careful characterization in the form of SEM (Fig. 11A) indicates that bacteria populate quite uniformly in the array without apparent mass transport issues. The cell loading of *S. ovata* within the nanowire array is 4.4 times that observed on a planar silicon electrode. From classical electrochemical analysis of the case without solar illumination (Fig. 11B), it was observed that the nanowire-bacteria hybrids are capable of reducing CO_2 to acetate under continuous sparging with 20% $\text{CO}_2/80\%$ N_2 with an overpotential less than 200 mV at 0 V vs. RHE. Additionally, the Tafel slope of bacteria-catalyzed CO_2 reduction is distinctly different from that of abiotic proton reduction, implying different reaction mechanisms. The overall system produced about 0.3 mA cm^{-2} photocurrent under simulated sunlight (AM 1.5G, 100 mW cm^{-2}) and was stable for more than 120 h; acetic acid was steadily produced with a product selectivity (Faradaic efficiency) of 86%, as shown in Fig. 11C. The acetic acid titers were ca. 1.2 g L^{-1} (20 mmol L^{-1}) after 5 days and could reach over 6 g L^{-1} (ca. 100 mmol L^{-1}) in M9-MOPS minimal medium. The resulting acetic acid can be activated to acetyl coenzyme A by genetically engineered *E. coli*, and the acetyl coenzyme A can be used as raw materials for various additional value chemicals such as *n*-butanol, polyhydroxybutyrate, and three different isoprenes [122,123].

Sakimoto et al. [124] reported the modification of non-photosynthetic heterotrophic bacteria (*Moorella thermoacetica*, *Mt*) by using cadmium sulfide (CdS) nanoparticles to

Fig. 10. (A) Scanning electron microscopy (SEM) images of Ni-PHF/CNT cathode; (B) Ni-PHF/CNT cathode with *S. ovata* biofilm on the surface of the cathodes; (C) LSV curves obtained for the Ni-PHF and Ni-PHF/CNT electrodes; (D) Electron transfer, measured acetate production, and current consumption of the Ni-PHF/CNT cathode [117].

Fig. 11. (A) Cross-sectional SEM image of the 3D network in the nanowire-bacteria hybrid; (B) Tafel plots; (C) Nonzero photocurrent [44].

construct a new PBS [125]. The researchers designed a bionic system based on “Z-scheme” in series. In the system shown in Fig. 12A, photoreduction and photooxidation were carried out by CdS and TiO₂ nanoparticles loaded with Mn (II) phthalocyanine (MnPc), respectively. Furthermore, light of wavelengths greater than 400 nm was successfully absorbed with the increase in the MnPc content on TiO₂. These two catalysts are linked by cystine/cysteine (Cyss/Cys), a biocompatible redox medium, which increases the electrical conductivity. On the cell surface, photoexcitation of the electrons released by the CdS nanoparticles produces a reduction equivalent [H]. Then, the CO₂ and [H] are reduced to acetic acid in the *W-L* pathway of *Mt*, which is photoreduction; photooxidation involves TiO₂ nanoparticles loaded with MnPc, which restore Cyss to Cys and oxidize water. The photoinduced holes are quenched by extracellular Cys [126]. In Fig. 12B, the photosynthetic properties of the *Mt*-CdS + TiO₂-MnPc tandem systems were compared with those of the control system, which produced more acetic acid. The rate of acetic acid formation tends to stabilize after about 1 day in the case of *Mt*-CdS system. The acetic acid yields of *Mt*-CdS and *Mt*-MnPc in the control system are both below the stoichiometric limits set by Cys as a limit preparation (dotted line, Cys-free optical regeneration). MnPc-free *Mt*-CdS TiO₂ and CdS-free *Mt* + TiO₂-MnPc series of systems display poor performances in terms of producing acetic acid.

3.2.2. Ethanol

Mohanakrishna et al. [17] used five different concentrations of enriched mixed homotype acetic acid-producing bacteria as cathodic biocatalysts to perform MES for reducing CO₂ into

Fig. 12. (A) Schematic of the *Mt*-CdS + TiO₂-MnPc tandem system; (B) Photosynthetic performance [124].

acetic acid and ethanol at a constant potential. With the increase in the carbon concentration, improvements in the acetate production rate and carbon conversion were observed. A maximum acetate production rate of 142.2 mg L⁻¹ per day and a maximum carbon conversion efficiency of 84% were achieved at the HCO₃⁻ concentrations of 4.0 g L⁻¹ and 2.5 g L⁻¹. The pH changes caused by the interaction between HCO₃⁻ (substrate) and acetate (products) can produce buffer properties at the cathode, which control the pH and substrate specificity during the MES process. At a higher concentration of acetic acid, the conditions for the reduction of acetic acid to ethanol can become more favorable, depending on the acidic pH environment. The maximum ethanol production of 65 mg L⁻¹ was observed at 4.0 g HCO₃⁻ L⁻¹.

Hydrogen produced from water electrolysis is an important medium for the electrochemical reduction of CO₂ at the cathode, and the supply of hydrogen also promotes the production of ethanol. Blanchet et al. [113] found that the acetic acid production of pure *S. ovata* culture grown under H₂ and CO₂ was up to 2904 mg L⁻¹. About 7 days later, ethanol production began and the acetic acid production plateaued. After 10 days of cultivation, an ethanol yield as high as 1411 mg L⁻¹ was obtained.

Li et al. [42] combined reverse electrodialysis technology with MES to develop a MREC for the first time. The researchers used the salinity gradient (composed of a high-concentration NaCl solution and a low-concentration NaCl solution) as the driving energy to realize the efficient biotransformation of CO₂ to value-added chemicals. The concentration of acetic acid increased gradually with time, reaching 7.33 mM, as shown in Fig. 13A, and the maximum concentration of ethanol was determined to be 39.1 mg L⁻¹, as shown in Fig. 13B. No acetic acid or ethanol was produced when *S. ovata* and the salinity gradient were not inoculated. In Fig. 13C and Fig. 13D, the injection of *S. ovata* enhances the current at the cathode, and the mechanism remains to be clarified. The cathodic potential stabilized at 0.680 V after 5.5 days, then, the current began to decrease,

Fig. 13. Feasibility of MREC on the conversion of CO₂ to acetate and ethanol [42]. The concentrations of (A) acetate and (B) ethanol as functions of time; (C) The current; (D) The cathodic potential during the CO₂ reduction process.

and the concentrations of acetic acid and ethanol reached the highest levels on the 6th day, as shown in Fig. 13A and Fig. 13B. After the reaction, the removal rate of COD and the Coulomb efficiency in the anode chamber reached 85.26% and 37.82%, respectively. This low Coulombic efficiency is possibly because the COD of wastewater could also be removed by the non-exoelectrogenic microorganisms present in wastewater. These results indicate that MERC is an alternative method of CO₂ conversion into value-added chemicals and wastewater treatment.

Biogenetic engineering is an efficient bioethanol production technology that combines solar energy conversion, carbon sequestration, and ethanol production [127]. Deng et al. [128] proved that ethanol can be produced from absorbed CO₂ by photosynthesis through metabolic engineering. *Synechocystis* sp. PCC 6803 is a heterotrophic cyanobacterium and is the first fully sequenced and annotated photosynthetic autotrophic organism [129]. Dexter et al. [130] reported the photoautotrophic *Synechocystis* sp. PCC 6803 that converted CO₂ into bioethanol. The ethanol-producing pyruvate decarboxylase of *Zymomonas mobilis* and ADH II genes were integrated into the chromosome of *Synechocystis* sp. PCC 6803 by using a double homologous recombination system. The ethanol concentration of the system reached 12 mM. Gao et al. [131] used *Synechocystis* sp. PCC 6803 to increase the yield of ethanol to 5.50 g L⁻¹. In 2017, Kopka et al. [132] systematically analyzed another ethanol-producing cyanobacterium *Synechococcus* sp. PCC 7002. They established an additional biosynthesis pathway in cyanobacteria host cells. The new ethanol-producing cyanobacteria engineering strain accumulated 0.25% (v/v) ethanol after 30 days of culturing.

3.3. C₂₊ compounds

The mechanisms of the formation of C₂₊ products from CO₂ artificial bioconversion are similar to those of the C₂ compounds, though much more complicated steps are involved. The key step in these carbon sequestration pathways that catalyze CO₂ fixation to produce C₂₊ compounds is the Calvin cycle. CO₂ and H₂ can be immobilized by the Calvin cycle to produce a variety of C₃₊ products, such as poly(3-hydroxybutyrate) (PHB) and C₃–C₅ alcohols. The Calvin cycle could even be combined with metabolic engineering to design reaction pathways for specific products such as isopropanol.

The aerobic microorganism *R. eutropha* without an organic growth substrate can use H₂ and CO₂ as its sole energy and carbon source and immobilize CO₂ through Calvin cycle, which is the main carbon sequestration pathway of the biosphere [133,134]. The ability of the OER at low overpotentials has been realized in the neutral pH range (6–8) with the development of cobalt phosphate (CoPi) catalyst. The OER catalyst shares many properties with the oxygen production catalyst in PSII, including its structure, self-assembling ability, self-repairing ability, low toxicity to bacteria, and good biocompatibility. More importantly, this kind of catalyst would not produce reactive oxygen species (ROS), resulting in a significant reduction in the voltage for water decomposition; the en-

ergy conversion efficiency is thus improved [19,135–137]. The resulting hydrogen can bound to CO₂ when the CoPi catalyst is coupled with the HER catalyst, which lays the foundation for the production of liquid and solid fuels [138].

3.3.1. PHB

Chong et al. [9] recently developed an efficient PBS consisting of cobalt phosphate | cobalt-phosphorus | *Ralstonia eutropha* (CoPi | Co-P | *R. eutropha*). At a low driving voltage, CoPi can decompose water into molecular hydrogen and oxygen and can store more than half of the energy of the input system in the form of a CO₂ reduction product. The products are PHB and C₃–C₅ alcohols. Entries 1, 2, 3, and 5 show that η_{elec} increases with decreasing E_{appl} below 100% CO₂ until $E_{appl} < 2.0$ V, as shown in Fig. 14A. Below $E_{appl} = 2.0$ V (entry 8), a higher salt concentration (108 entries for phosphate buffer) is required to facilitate mass transport and the attendant current. However, high salt concentrations are undesirable for *R. eutropha* metabolism. The results show that at the optimal phosphate concentration of 36 mM and $E_{appl} = 2.0$ V, the highest biomass yield was 54% (entry 5) for a duration of 6 days. This biomass yield is equivalent to assimilating ca. 4.1 mol (180 g) of CO₂ with 1 kWh of electricity. Enlarging the batch reactor volume by a factor of 10 did not affect the efficiency (entries 4 and 6), indicating that the system is scalable and that the reactor volume is not limited. They found that the biomass accumulation scales linearly with the amount of charge passed under pure CO₂ atmosphere (Fig. 14B) or at ambient CO₂ levels (Fig. 14C). The biomass accumulation increases linearly with the increase in the charge, and the linear growth conditions are similar, indicating that the oxidation of hydrogen is the decisive step in the bioelectrical-assisted synthesis process. *R. eutropha* stops growing in the dark cycle and resumes water cracking and con-

Fig. 14. (A) η_{elec} values for the production of biomass and chemicals at different values of E_{appl} and for various configurations; (B) Biomass accumulation (OD₆₀₀) and amounts of electric charges that were passed; (C) Real-time monitoring of the biomass accumulation [9].

tinuous reduction of CO_2 in the light cycle after 12 h (Fig. 14C), which indicates that the $\text{CoPi} \mid \text{Co-P} \mid R. eutropha$ system can adapt to the intermittency of solar energy. Coupled with the existing photovoltaic system, the energy efficiency is about 50%, which can produce about 10% CO_2 emission reduction efficiency, which exceeds the energy efficiency of the natural photosynthetic system.

To avoid the potentially toxic effect of ROS on cell growth, Chen et al. [139] adopted a two-chamber bioelectrochemical reactor, in which the *R. eutropha* in the cathodic chamber was separated from the anodic chamber by a proton exchange membrane (PEM). Thus, the ROS produced in the anodic chamber could not penetrate the PEM, which prevented its entry into the cathodic chamber that can poison the cells. To improve the efficiency of CO_2 reduction to formate, the researchers constructed an enzyme-assisted NR-mediated MES system by incorporating FDH, which offered two advantages over indium foil cathode for formate formation. On one hand, the cathode potential was only -0.6 V (vs. Ag/AgCl), which was much higher than the -1.6 V (vs. Ag/AgCl) for the system of inorganic electrocatalysts. Thus, the electrical power consumption could be tremendously reduced at such a low overpotential. On the other hand, the electron transport from the cathode into *R. eutropha* was increased, since NR played the role of an electron shuttle and formate acted as an electron carrier. The reduced NR diffused directly into *R. eutropha* through pathway I (electron transfer mechanism mediated by NR), thus increasing the level of intracellular reduction equivalents and further improving the efficiency of MES. NR also promoted the extracellular regeneration of NADH and effectively promoted the reduction of CO_2 to formic acid, catalyzed by FDH, in the cathode chamber. Formic acid then transferred to *R. eutropha* via pathway II (formic acid-mediated electron transfer mechanism) as an electron carrier, and an efficient CBB cycle devel-

Fig. 15. (A) Schematic of FDH-assisted MES to reduce CO_2 to synthesize PHB; (B) PHB yields in WT *R. eutropha* and RuBisCO-overexpressed *R. eutropha*; (C) Enhancement in PHB production with gradual optimization of the MES process [139].

oped by the heterologous expression of RuBisCO to synthesize PHB, as shown in Fig. 15A [140]. 485 mg L^{-1} of PHB was synthesized by the RuBisCO overexpressed *R. eutropha*, while only 383 mg L^{-1} of PHB was synthesized by WT *R. eutropha* (Fig. 15B). In Fig. 14C, 0.05 mM NR was added to MES; WT *R. eutropha* produced 226 mg L^{-1} PHB. However, when *R. eutropha* was introduced into RuBisCO, only 156 mg L^{-1} of PHB accumulated. With the incorporation of FDH, 485 mg L^{-1} of PHB could be synthesized by *R. eutropha* in the FDH-assisted MES system. 383 mg L^{-1} of PHB was synthesized by WT *R. eutropha*.

3.3.2. Isopropanol

Torella et al. [10] designed an integrated inorganic-biological hybrid system to achieve an overall efficiency comparable to or exceeding that of a natural system at low overpotentials. In this work, the system has been engineered based on the CoPi water-splitting anode, with NiMoZn or stainless-steel (304 mesh 60) as the cathode, to generate H_2 by electrolysis of water. The biosynthetic process of isopropanol ($(\text{CH}_3)_2\text{CHOH}$) is shown in Fig. 16A; *R. eutropha* H16 oxidizes H_2 with hydrogenases to produce NADPH and ATP. Then, CO_2 is reduced to 3-phosphoglycerate (3PG) by Calvin cycle. The 3PG is rapidly converted to PHB by acetyl-coenzyme A as follow. In the synthesis of PHB, the strain Re2133-pEG12 was destroyed and four genes that redirected acetyl-coenzyme A to synthesize isopropanol were expressed. Plasmid pEG12 expressed genes from ketosulfide (*phaA**) and acetic acid-CoA transferase (*ctf*) of *R. eutropha*, as well as acetoacetic acid decarboxylase and ADH from *Clostridium* sp. Through the action of these enzymes, 3PG is transferred to isopropanol in Re2133-pEG12 (Fig. 16B). The yield of isopropanol was 216 mg L^{-1} after 5 days, and the

Fig. 16. (A) Engineered pathway for isopropanol production; (B) Growth and isopropanol production in *Re2133-pEG12* grown at 3.0 V [10].

byproducts pyruvate (17 mg L⁻¹) and acetone (10 mg L⁻¹) were also produced, with the maximum bioelectrochemical efficiency being 3.9%.

3.3.3. Acetone

Ketones are important organic compounds. Acetone, as the simplest ketone, is widely used as a solvent or precursor of industrial chemicals. Zhou et al. [141] reported a biological process using CO₂ to produce acetone (CH₃COCH₃). An exogenous CO₂ synthesis pathway was introduced into *Synechocystis* sp. PCC 6803 to construct the modular synthesis pathway of acetone biosynthesis. In this work, 36.0 mg L⁻¹ acetone could be produced. Li et al. [142] designed a kind of *R. eutropha* H16 in the electro-bioreactor that can fix CO₂ through genetic engineering. The produced fuel yield was more than 1.4 g L⁻¹ (~846 mg L⁻¹ isobutanol and ~570 mg L⁻¹ 3-methyl-1-butanol).

3.3.4. Butyric acid

Ganigué et al. [143] demonstrated for the first time the bioelectrochemical synthesis of butyric acid (CH₃(CH₂)₂COOH) by using CO₂ as the sole carbon source. The maximum concentration of butyric acid was 20.2 mM, and the maximum yield 1.82 mM d⁻¹. Production of bioethanol (ethanol and butanol) from CO₂ was also observed. In 2017, Battle-Vilanova et al. [144] used the tubular bioelectrochemical system and mixed cultured microbial community to increase the yield of butyric acid. The authors suggested that chain extension with acetic acid and ethanol as the main raw materials was the main hypothesis for the production of butyric acid. The maximum yield of butyric acid was 7.2 mmol L⁻¹ d⁻¹, and the concentration of butyric acid was up to 252.4 mmol L⁻¹. when tested at a fixed cathodic potential of -0.8 V (vs. SHE). The yields of other products (acetic acid, ethanol, and butanol) were low.

3.3.5. Isoprene

Isoprene (CH₂C(CH₃)CHCH₂) is an important component of synthetic rubber, which is produced entirely from petrochemical raw materials. Previous studies on metabolic engineering mainly focused on the heterologous expression of metabolic pathways [145–147]. In order to directly produce isoprene from CO₂, Gao et al. [148] developed the methylerythritol phosphate biosynthesis pathway for isoprene in cyanobacteria in 2016. The isoprene synthetase with a high activity from plants was used to improve the production activity of isoprene. The engineering strain orientated about 40% of the photosynthetically fixed carbon to the isoprene biosynthesis pathway and produced 1.26 g L⁻¹ of isoprene from CO₂.

4. Conclusions and perspectives

This paper summarized the recent progresses in CO₂ artificial biotransformation. The key techniques, including microbial electrosynthesis, photosynthetic biohybrid systems, PSII hybrid system, and metabolic engineering, were introduced. The various chemicals synthesized from these techniques were discussed in detail from the aspects of hybrid systems and the possible mechanisms.

On the basis of the current status of CO₂ artificial bioconversion, we present several future prospects and directions for possible applications.

(1) The electron transfer mechanism involved in the process of CO₂ artificial biotransformation has not been confirmed, and this process has not been understood clearly and in-depth. Only by mastering these core disciplines and reaction mechanisms can we design and construct an efficient artificial biotransformation system for CO₂. Only then can we really promote the research of sustainable energy production and solve the environmental problem associated with CO₂.

(2) CO₂ is a very stable molecule and its activation is a fundamental challenge because the carbon atom in the molecule is in the highest oxidation state, that is, it is in the lowest energy state. The process of converting inorganic carbon to organic carbon requires a lot of energy and reducing power. According to the standard redox potential shown in equations (1)–(6) and the multi-electron reduction steps of CO₂, the products of CO₂ reduction can be transformed to different compounds and target products with different carbon chain lengths can be obtained.

(3) We should fully develop efficient catalysts that are composed of earth-abundant elements. These catalysts should display the advantages of low cost, good biocompatibility, high conductivity, high specific surface area, and generality. This is an important prerequisite to realize large-scale conversion and utilization of CO₂ with renewable energy.

(4) By understanding the diversity of carbon sequestration organisms and their metabolic pathways in nature and discovering efficient carbon sequestration elements, microorganisms can be modified with various metabolic pathways to realize the design of a carbon sequestration pathway of converting CO₂ to target products.

Research on artificial biotransformation of CO₂ has been growing, and great breakthroughs have been made in related fields. This important technology will make use of the most extensive renewable resource on the planet, CO₂, to address the environmental and energy problems efficiently and in a green fashion. In the future, biocompatible solid-state nano-devices can be combined with living systems, and the acetic acid obtained through artificial bioconversion of CO₂ can continue to be activated to acetoacetyl-CoA by downstream genetically engineered *E.coli* and used as a building block for a variety of value-added chemicals such as n-butanol, PHB polymer, and three different isoprenoid natural products.

References

- [1] U. N., World Economic Situation and Prospects (Zhongguo Caizheng), **2018**.
- [2] B. C. O'Neill, M. Oppenheimer, *Science*, **2002**, 296, 1971–1972.
- [3] J. Wu, X. D. Zhou, *Chin. J. Catal.*, **2016**, 37, 999–1015.
- [4] B. James, *Chem. Soc. Rev.*, **2009**, 38, 185–196.
- [5] H. Li, J. C. Liao, *Energy Environ. Sci.*, **2013**, 6, 2892–2899.
- [6] L. Wei, Q. Wang, Y. Xin, Y. Lu, J. Xu, *Algal Res.*, **2017**, 27, 366–375.
- [7] C. Wu, Y. Zhou, Z. Zou, *Chin. J. Catal.*, **2011**, 32, 1565–1572.
- [8] L. Shi, G. H. Yang, K. Tao, Y. Yoneyama, Y. S. Tan, N. Tsubaki, *Acc. Chem. Res.*, **2013**, 48, 1838–1847.

Graphical Abstract

Chin. J. Catal., 2019, 40: 1421–1437 doi: S1872-2067(19)63408-X

Artificial bioconversion of carbon dioxide

Ting-Ting Zhao, Guang-Hui Feng, Wei Chen*, Yan-Fang Song, Xiao Dong, Gui-Hua Li, Hai-Jiao Zhang, Wei Wei*
Shanghai University; Shanghai Advanced Research Institute, Chinese Academy of Sciences; ShanghaiTech University

The CO₂ artificial bioconversion system, in which CO₂ is converted into value-added chemicals via the metabolic pathway in organisms, is driven by renewable energy.

- [9] C. Liu, B. C. Colon, M. Ziesack, P. A. Silver, D. G. Nocera, *Science*, **2016**, 352, 1210–1213.
- [10] J. P. Torella, C. J. Gagliardi, J. S. Chen, D. K. Bediako, B. Colón, J. C. Way, P. A. Silver, D. G. Nocera, *Proc. Natl. Acad. Sci. U. S. A.*, **2015**, 112, 2337–2342.
- [11] M. Schreier, L. Curvat, F. Giordano, L. Steier, A. Abate, S. M. Zakee-ruddin, J. Luo, M. T. Mayer, M. Grätzel, *Nat. Commun.*, **2015**, 6 (7326), 1–6.
- [12] M. Schreier, F. Héroguel, L. Steier, S. Ahmad, J. S. Luterbacher, M. T. Mayer, J. Luo, M. Grätzel, *Nat. Energy*, **2017**, 2 (17087), 1–9.
- [13] S. Liu, H. Tao, Q. Liu, Z. Xu, Q. Liu, J.-L. Luo, *ACS Catal.*, **2018**, 8, 1469–1475.
- [14] X. Zheng, B. Zhang, P. De Luna, Y. Liang, R. Comin, O. Voznyy, L. Han, F. P. G. de Arquer, M. Liu, C. T. Dinh, T. Regier, J. J. Dynes, S. He, H. L. Xin, H. Peng, D. Prendergast, X. Du, E. H. Sargent, *Nat. Chem.*, **2018**, 10, 149–154.
- [15] S. Liu, J. Xiao, X. F. Lu, J. Wang, X. Wang, X. W. Lou, *Angew. Chem. Int. Ed.*, **2019**, 58, 8499–8503.
- [16] H. J. Shin, K. A. Jung, C. W. Nam, J. M. Park, *Bioresour. Technol.*, **2017**, 245, 1421–1429.
- [17] G. Mohanakrishna, K. Vanbroekhoven, D. Pant, *React. Chem. Eng.*, **2018**, 3, 371–378.
- [18] S. Bajracharya, S. Srikanth, G. Mohanakrishna, R. Zacharia, D. P. B. T. B. Strik, D. Pant, *J. Power Sources*, **2017**, 356, 256–273.
- [19] K. P. Nevin, T. L. Woodard, A. E. Franks, Z. M. Summers, D. R. Lovley, *Mbio*, **2010**, 1, e00103-10/1-e00103-10/4, doi: 10.1128/mBio.00103-10.
- [20] K. K. Sakimoto, N. Kornienko, P. Yang, *Acc. Chem. Res.*, **2017**, 50, 476–481.
- [21] X. Christodoulou, T. Okoroafor, S. Parry, S. B. Velasquez-Orta, *J. CO₂ Util.*, **2017**, 18, 390–399.
- [22] X. Christodoulou, S. B. Velasquez-Orta, *Environ. Sci. Technol.*, **2016**, 50, 11234–11242.
- [23] P. Zhang, Y. Yang, J. Shi, Y. Zheng, L. Wang, X. Li, *Renew. Sustain. Energy Rev.*, **2009**, 13, 439–449.
- [24] R. E. Blankenship, D. M. Tiede, J. Barber, G. W. Brudvig, G. Fleming, M. Ghirardi, M. R. Gunner, W. Junge, D. M. Kramer, A. Melis, T. A. Moore, C. C. Moser, D. G. Nocera, A. J. Nozik, D. R. Ort, W. W. Parson, R. C. Prince, R. T. Sayre, *Science*, **2011**, 332, 805–809.
- [25] T. Zhang, *Science*, **2015**, 350, 738–739.
- [26] H. W. Zhu, Y. P. Zhang, Y. Li, *Sci. Sin. Vitae*, **2016**, 46, 1388–1399.
- [27] P. Gao, S. Li, X. Bu, S. Dang, Z. Liu, H. Wang, L. Zhong, M. Qiu, C. Yang, J. Cai, W. Wei, Y. Sun, *Nat. Chem.*, **2017**, 9, 1019–1024.
- [28] P.-L. Tremblay, T. Zhang, *Front. Microbiol.*, **2015**, 6, 201/1–201/10.
- [29] J. Du, C. Catania, G. C. Bazan, *Chem. Mater.*, **2014**, 26, 686–697.
- [30] T. Zhang, H. Nie, T. S. Bain, H. Lu, M. Cui, O. L. Snoeyenbos-West, A. E. Franks, K. P. Nevin, T. P. Russell, D. R. Lovley, *Energy Environ. Sci.*, **2013**, 6, 217–224.
- [31] K. P. Nevin, S. A. Hensley, A. E. Franks, Z. M. Summers, J. Ou, T. L. Woodard, O. L. Snoeyenbos-West, D. R. Lovley, *Appl. Environ. Microbiol.*, **2011**, 77, 2882–2886.
- [32] J. Sadhukhan, J. R. Lloyd, K. Scott, G. C. Premier, E. H. Yu, T. Curtis, I. M. Head, *Renew. Sustain. Energy Rev.*, **2016**, 56, 116–132.
- [33] S. Bajracharya, A. ter Heijne, X. D. Benetton, K. Vanbroekhoven, C. J. N. Buisman, D. P. B. T. B. Strik, D. Pant, *Bioresour. Technol.*, **2015**, 195, 14–24.
- [34] C. W. Marshall, D. E. Ross, E. B. Ficht, N. S. Norman, H. D. May, *Environ. Sci. Technol.*, **2013**, 47, 6023–6029.
- [35] L. Jourdin, S. Freguia, B. C. Donose, J. Chen, G. G. Wallace, J. Keller, V. Flexer, *J. Mater. Chem. A*, **2014**, 2, 13093–13102.
- [36] V. Flexer, J. Chen, B. C. Donose, P. Sherrell, G. G. Wallace, J. Keller, *Energy Environ. Sci.*, **2013**, 6, 1291–1298.
- [37] N. S. Malvankar, D. R. Lovley, *Curr. Opin. Biotechnol.*, **2014**, 27, 88–95.
- [38] K. K. Sakimoto, C. Liu, J. Lim, P. Yang, *Nano Lett.*, **2014**, 14, 5471–5476.
- [39] H. E. Jeong, I. Kim, P. Karam, H.-J. Choi, P. Yang, *Nano Lett.*, **2013**, 13, 2864–2869.
- [40] G. Z. Ramon, B. J. Feinberg, E. M. V. Hoek, *Energy Environ. Sci.*, **2011**, 4, 4423–4434.
- [41] R. D. Cusick, Y. Kim, B. E. Logan, *Science*, **2012**, 335, 1474–1477.
- [42] X. Li, I. Angelidaki, Y. Zhang, *Water Res.*, **2018**, 142, 396–404.
- [43] C. Liu, J. Tang, H. M. Chen, B. Liu, P. Yang, *Nano Lett.*, **2013**, 13, 2989–2992.
- [44] C. Liu, J. J. Gallagher, K. K. Sakimoto, E. M. Nichols, C. J. Chang, M. C. Y. Chang, P. Yang, *Nano Lett.*, **2015**, 15, 3634–3639.
- [45] N. Kornienko, K. K. Sakimoto, D. M. Herlihy, S. C. Nguyen, A. P. Alivisatos, C. B. Harris, A. Schwartzberg, P. Yang, *Proc. Natl. Acad. Sci. U. S. A.*, **2016**, 113, 11750–11755.
- [46] Y. Amao, R. Kataoka, *Catal. Today*, **2018**, 307, 243–247.
- [47] R. K. Yadav, J.-O. Baeg, A. Kumar, K.-J. Kong, G. H. Oh, N.-J. Park, *J. Mater. Chem. A*, **2014**, 2, 5068–5076.
- [48] N. Aryal, A. Halder, P.-L. Tremblay, Q. Chi, T. Zhang, *Electrochim. Acta*, **2016**, 217, 117–122.
- [49] Y. Li, *Sci. China Mater.*, **2016**, 59, 93–94.

- [50] W. Wang, J. Chen, C. Li, W. Tian, *Nat. Commun.*, **2014**, 5, 4647/1–4647/8.
- [51] K. Sauer, V. K. Yachandra, *Biochim. Biophys. Acta-Bioenerg.*, **2004**, 1655, 140–148.
- [52] Y. N. Wang, C. X. Zhang, L. Wang, J. Q. Zhao, *Chin. Sci. Bull.*, **2013**, 58, 3213–3216.
- [53] W. Wang, Z. Wang, Q. Zhu, G. Han, C. Ding, J. Chen, J. R. Shen, C. Li, *Chem. Commun.*, **2015**, 51, 16952–16955.
- [54] W. Wang, Z. Li, J. Chen, C. Li, *J. Phy. Chem. C*, **2017**, 121, 2605–2612.
- [55] S. Ye, C. Ding, R. Chen, F. Fan, P. Fu, H. Yin, X. Wang, Z. Wang, P. Du, C. Li, *J. Am. Chem. Soc.*, **2018**, 140, 3250–3256.
- [56] F. Wen, C. Li, *Acc. Chem. Res.*, **2013**, 46, 2355–2364.
- [57] Y. Li, *Chin. J. Biotechnol.*, **2009**, 25, 1281–1284.
- [58] J. E. Bailey, *Science*, **1991**, 252, 1668–1675.
- [59] M. Koffas, C. Roberge, K. Lee, G. Stephanopoulos, *Ann. Rev. Biomed. Eng.*, **1999**, 1, 535–557.
- [60] T. Minowa, S. Yokoyama, M. Kishimoto, T. Okakura, *Fuel*, **1995**, 74, 1735–1738.
- [61] S. Hirayama, R. Ueda, Y. Ogushi, A. Hirano, Y. Samejima, K. Hon-Nami, S. Kunito, *Stud. Surf. Sci. Catal.*, **1998**, 114, 657–660.
- [62] L. Wei, Y. Xin, Q. Wang, J. Yang, H. Hu, J. Xu, *Plant J.*, **2017**, 89, 1236–1250.
- [63] M. Liu, Y. Ding, H. Chen, Z. Zhao, H. Liu, M. Xian, G. Zhao, *BMC Microbiol.*, **2017**, 17, 10/1–10/9.
- [64] F. Gong, Z. Cai, Y. Li, *Sci. China Life Sci.*, **2016**, 59, 1106–1114.
- [65] A. Bar-Even, E. Noor, N. E. Lewis, R. Milo, *Proc. Natl. Acad. Sci. U. S. A.*, **2010**, 107, 8889–8894.
- [66] M. S. Khan, *Trends Biotechnol.*, **2007**, 25, 437–440.
- [67] Y. Marcus, H. Altman-Gueta, Y. Wolff, M. Gurevitz, *J. Exp. Bot.*, **2011**, 62, 4173–4182.
- [68] D. M. Kramer, J. R. Evans, *Plant Physiol.*, **2011**, 155, 70–78.
- [69] J. R. Evans, *Plant Physiol.*, **2013**, 162, 1780–1793.
- [70] J. Zhou, F. Zhang, H. Meng, Y. Zhang, Y. Li, *Metab. Eng.*, **2016**, 38, 217–227.
- [71] F. Liang, P. Lindblad, *Metab. Eng. Commun.*, **2017**, 4, 29–36.
- [72] E. Herz, N. Antonovsky, Y. Bar-On, D. Davidi, S. Gleizer, N. Prywes, L. Noda-Garcia, K. L. Frisch, Y. Zohar, D. G. Wernick, A. Savidor, U. Barenholz, R. Milo, *Nat. Commun.*, **2017**, 8, 1705/1–1705/10.
- [73] N. Antonovsky, S. Gleizer, E. Noor, Y. Zohar, E. Herz, U. Barenholz, L. Zelcbuch, S. Amram, A. Wides, N. Tepper, D. David, Y. Bar-On, T. Bareis, D. G. Wernick, I. Shani, S. Malitsky, G. Jona, A. Bar-Even, R. Milo, *Cell*, **2016**, 166, 115–125.
- [74] T. O. Yeates, N. M. Wheatley, *Science*, **2017**, 358, 1253–1254.
- [75] H. Aigner, R. H. Wilson, A. Bracher, L. Calisse, J. Y. Bhat, F. U. Hartl, M. Hayer-Hartl, *Science*, **2017**, 358, 1272–1278.
- [76] S. Schlager, A. Fuchsbaauer, M. Haberbauer, H. Neugebauer, N. S. Sariciftci, *J. Mater. Chem. A*, **2017**, 5, 2429–2443.
- [77] F. Marpani, M. Pinelo, A. S. Meyer, *Biochem. Eng. J.*, **2017**, 127, 217–228.
- [78] K. Kalyanasundaram, M. Graetzel, *Curr. Opin. Biotechnol.*, **2010**, 21, 298–310.
- [79] Y. Surendranath, D. K. Bediako, D. G. Nocera, *Proc. Natl. Acad. Sci. U. S. A.*, **2012**, 109, 15617–15621.
- [80] D. G. Nocera, *Acc. Chem. Res.*, **2012**, 45, 767–776.
- [81] G. A. Olah, A. Goepfert, G. K. S. Prakash, *Beyond Oil and Gas: The Methanol Economy*, 2nd ed., Wiley-VCH, Weinheim, **2009**.
- [82] R. Obert, B. C. Dave, *J. Am. Chem. Soc.*, **1999**, 121, 12192–12193.
- [83] S.-W. Xu, Y. Lu, J. Li, Z.-Y. Jiang, H. Wu, *Ind. Eng. Chem. Res.*, **2006**, 45, 4567–4573.
- [84] M. Aresta, A. Dibenedetto, C. Pastore, *Environ. Chem. Lett.*, **2005**, 3, 113–117.
- [85] P. K. Addo, R. L. Arechederra, S. D. Minter, *Electroanalysis*, **2010**, 22, 807–812.
- [86] J.-H. Jeoung, H. Dobbek, *Science*, **2007**, 318, 1461–1464.
- [87] M. Villano, F. Aulenta, C. Ciucci, T. Ferri, A. Giuliano, M. Majone, *Bioresource Technol.*, **2010**, 101, 3085–3090.
- [88] S. Cheng, D. Xing, D. F. Call, B. E. Logan, *Environ. Sci. Technol.*, **2009**, 43, 3953–3958.
- [89] S. Schlager, L. M. Dumitru, M. Haberbauer, A. Fuchsbaauer, H. Neugebauer, D. Hiemetsberger, A. Wagner, E. Portenkirchner, N. S. Sariciftci, *ChemSusChem*, **2016**, 9, 631–635.
- [90] T. W. Woolerton, S. Sheard, E. Pierce, S. W. Ragsdale, F. A. Armstrong, *Energy Environ. Sci.*, **2011**, 4, 2393–2399.
- [91] T. W. Woolerton, S. Sheard, E. Reisner, E. Pierce, S. W. Ragsdale, F. A. Armstrong, *J. Am. Chem. Soc.*, **2010**, 132, 2132–2133.
- [92] L. Dan, G. Feng, S. Fan, *J. Microbiol.*, **2003**, 23(6), 42–46.
- [93] K. Manthiram, B. J. Beberwyck, A. P. Alivisatos, *J. Am. Chem. Soc.*, **2014**, 136, 13319–13325.
- [94] Y. Hori, I. Takahashi, O. Koga, N. Hoshi, *J. Phys. Chem. B*, **2002**, 106, 15–17.
- [95] S. Cheng, D. Xing, D. F. Call, B. E. Logan, *Environ. Sci. Technol.*, **2009**, 43, 3953–3958.
- [96] E. M. Nichols, J. J. Gallagher, C. Liu, Y. Su, J. Resasco, Y. Yu, Y. Sun, P. Yang, M. C. Y. Chang, C. J. Chang, *Proc. Natl. Acad. Sci. U. S. A.*, **2015**, 112, 11461–11466.
- [97] J. Song, Y. Kim, M. Lim, H. Lee, J. I. Lee, W. Shin, *ChemSusChem*, **2011**, 4, 587–590.
- [98] S. Y. Lee, S. Y. Lim, D. Seo, J.-Y. Lee, T. D. Chung, *Adv. Energy Mater.*, **2016**, 6, 1502207.
- [99] J. Shi, C. Yang, S. Zhang, X. Wang, Z. Jiang, W. Zhang, X. Song, Q. Ai, C. Tian, *ACS Appl. Mater. Interfaces*, **2013**, 5, 9991–9997.
- [100] D. R. Dreyer, D. J. Miller, B. D. Freeman, D. R. Paul, C. W. Bielawski, *Chem. Sci.*, **2013**, 4, 3796–3802.
- [101] K. Kang, S. Lee, R. Kim, I. S. Choi, Y. Nam, *Angew. Chem. Int. Ed.*, **2012**, 51, 13101–13104.
- [102] F. Jin, X. Zeng, J. Liu, Y. Jin, L. Wang, H. Zhong, G. Yao, Z. Huo, *Sci. Rep.*, **2014**, 4, 4503/1–4503/8.
- [103] N. S. Lewis, D. G. Nocera, *Proc. Natl. Acad. Sci. U. S. A.*, **2006**, 103, 15729–15735.
- [104] Y. Amao, M. Fujimura, M. Miyazaki, A. Tadokoro, M. Nakamura, N. Shuto, *New J. Chem.*, **2018**, 42, 9269–9280.
- [105] J. Liu, R. Cazelles, Z. P. Chen, H. Zhou, A. Galarneau, M. Antonietti, *Phys. Chem. Chem. Phys.*, **2014**, 16, 14699–14705.
- [106] K. Ma, O. Yehezkeli, E. Park, J. N. Cha, *ACS Catal.*, **2016**, 6, 6982–6986.
- [107] R. K. Yadav, G. H. Oh, N.-J. Park, A. Kumar, K. Kong, J.-O. Baeg, *J. Am. Chem. Soc.*, **2014**, 136, 16728–16731.
- [108] R. K. Yadav, J. O. Baeg, G. H. Oh, N. J. Park, K. Kong, J. Kim, D. W. Hwang, S. K. Biswas, *J. Am. Chem. Soc.*, **2012**, 134, 11455–11461.
- [109] Y. Xu, Z. Liu, X. Zhang, Y. Wang, J. Tian, Y. Huang, Y. Ma, X. Zhang, Y. Chen, *Adv. Mater.*, **2009**, 21, 1275–1279.
- [110] O. Heichal-Segal, S. Rappoport, S. Braun, *Bio/Technology*, **1995**, 13, 798–800.
- [111] Z. Lian, D. Pan, W. Wang, D. Zhang, G. Li, H. Li, *J. Environ. Sci.*, **2017**, 60, 108–113.
- [112] H. Huber, M. Gallenberger, U. Jahn, E. Eylert, I. A. Berg, D. Kockelkorn, W. Eisenreich, G. Fuchs, *Proc. Natl. Acad. Sci. U. S. A.*, **2008**, 105, 7851–7856.
- [113] E. Blanchet, F. Duquenne, Y. Rafrafi, L. Etcheverry, B. Erable, A. Bergel, *Energy Environ. Sci.*, **2015**, 8, 3731–3744.
- [114] F. Ammam, P.-L. Tremblay, D. M. Lizak, T. Zhang, *Biotechnol. Biofuels*, **2016**, 9, 163/1–163/10.
- [115] H. Nie, T. Zhang, M. Cui, H. Lu, D. R. Lovley, T. P. Russell, *Phys. Chem. Chem. Phys.*, **2013**, 15, 14290–14294.

- [116] T. Song, K. Fei, H. Zhang, H. Yuan, Y. Yang, P. Ouyang, J. Xie, *J. Chem. Technol. Biotechnol.*, **2018**, 93, 457–466.
- [117] B. Bian, M. F. Alqahtani, K. P. Katuri, D. Liu, S. Bajracharya, Z. Lai, K. Rabaey, P. E. Saikaly, *J. Mater. Chem. A*, **2018**, 6, 17201–17211.
- [118] C. Lu, H. Bai, B. Wu, F. Su, J. F. Hwang, *Energy Fuels*, **2008**, 22, 3050–3056.
- [119] M. Rahimi, J. K. Singh, F. Müller-Plathe, *J. Phys. Chem. C*, **2015**, 119, 15232–15239.
- [120] M. Rahimi, J. K. Singh, D. J. Babu, J. J. Schneider, F. Müller-Plathe, *J. Phys. Chem. C*, **2013**, 117, 13492–13501.
- [121] Y. Zheng, Y. Jiao, Y. Zhu, H. L. Li, Y. Han, Y. Chen, A. Du, M. Jaroniec, S. Z. Qiao, *Nat. Commun.*, **2014**, 5, 3783/1–3783/8.
- [122] M. C. Y. Chang, R. A. Eachus, W. Trieu, D.-K. Ro, J. D. Keasling, *Nat. Chem. Biol.*, **2007**, 3, 274–277.
- [123] J. D. Keasling, *Science*, **2010**, 330, 1355–1358.
- [124] K. K. Sakimoto, S. J. Zhang, P. Yang, *Nano Lett.*, **2016**, 16, 5883–5887.
- [125] V. Mueller, *Science*, **2016**, 351, 34.
- [126] K. K. Sakimoto, A. B. Wong, P. Yang, *Science*, **2016**, 351, 74–77.
- [127] A. Hirano, R. Ueda, S. Hirayama, Y. Ogushi, *Energy*, **1997**, 22, 137–142.
- [128] M. De Deng, J. R. Coleman, *Appl. Environ. Microbiol.*, **1999**, 65, 523–528.
- [129] T. Kaneko, S. Tabata, *Plant Cell Physiol.*, **1997**, 38, 1171–1176.
- [130] J. Dexter, P. Fu, *Energy Environ. Sci.*, **2009**, 2, 857–864.
- [131] Z. Gao, H. Zhao, Z. Li, X. Tan, X. Lu, *Energy Environ. Sci.*, **2012**, 5, 9857–9865.
- [132] J. Kopka, S. Schmidt, F. Dethloff, N. Pade, S. Berendt, M. Schottkowski, N. Martin, U. Dühring, E. Kuchmina, H. Enke, *Biotechnol. Biofuels*, **2017**, 10, 56/1–56/21.
- [133] A. Pohlmann, W. F. Fricke, F. Reinecke, B. Kusian, H. Liesegang, R. Cramm, T. Eitinger, C. Ewering, M. Pötter, E. Schwartz, A. Strittmatter, I. Voß, G. Gottschalk, A. Steinbüchel, B. Friedrich, B. Bowien, *Nat. Biotechnol.*, **2006**, 24, 1257–1262.
- [134] M. Calvin, A. A. Benson, *Science*, **1949**, 109, 140–142.
- [135] A. J. Esswein, Y. Surendranath, S. Y. Reece, D. G. Nocera, *Energy Environ. Sci.*, **2011**, 4, 499–504.
- [136] D. R. Lovley, *Environ. Microbiol. Rep.*, **2011**, 3, 27–35.
- [137] K. Rabaey, R. A. Rozendal, *Nat. Rev. Microbiol.*, **2010**, 8, 706–716.
- [138] S. Y. Reece, J. A. Hamel, K. Sung, T. D. Jarvi, A. J. Esswein, J. J. H. Pijpers, D. G. Nocera, *Science*, **2011**, 334, 645–648.
- [139] X. Chen, Y. Cao, F. Li, Y. Tian, H. Song, *ACS Catal.*, **2018**, 8, 4429–4437.
- [140] G. G. B. Tcherkez, G. D. Farquhar, T. J. Andrews, *Proc. Natl. Acad. Sci. U. S. A.*, **2006**, 103, 7246–7251.
- [141] J. Zhou, H. Zhang, Y. Zhang, Y. Li, Y. Ma, *Metab. Eng.*, **2012**, 14, 394–400.
- [142] H. Li, P. H. Opgenorth, D. G. Wernick, S. Rogers, T.-Y. Wu, W. Higashide, P. Malati, Y.-X. Huo, K. M. Cho, J. C. Liao, *Science*, **2012**, 335, 1596.
- [143] R. Ganigué, S. Puig, P. Batlle-Vilanova, M. D. Balaguer, J. Colprim, *Chem. Commun.*, **2015**, 51, 3235–3238.
- [144] P. Batlle-Vilanova, R. Ganigué, S. Ramió-Pujol, L. Bañeras, G. Jiménez, M. Hidalgo, M. D. Balaguer, J. Colprim, S. Puig, *Bioelectrochemistry*, **2017**, 117, 57–64.
- [145] E. I. Lan, J. C. Liao, *Metab. Eng.*, **2011**, 13, 353–363.
- [146] V. J. J. Martin, D. J. Pitera, S. T. Withers, J. D. Newman, J. D. Keasling, *Nat. Biotechnol.*, **2003**, 21, 796–802.
- [147] P. Lindberg, S. Park, A. Melis, *Metab. Eng.*, **2010**, 12, 70–79.
- [148] X. Gao, F. Gao, D. Liu, H. Zhang, X. Nie, C. Yang, *Energy Environ. Sci.*, **2016**, 9, 1400–1411.

二氧化碳的人工生物转化

赵婷婷^{a,b}, 冯光辉^{a,b}, 陈为^{b,*}, 宋艳芳^b, 董笑^b, 李桂花^b, 张海娇^a, 魏伟^{b,c,#}

^a上海大学环境与化学工程学院, 上海200444

^b中国科学院上海高等研究院, 中国科学院低碳转化科学与工程重点实验室, 上海201210

^c上海科技大学物质科学与技术学院, 上海201210

摘要: CO₂是最主要的温室气体,也是重要的碳氧资源。从资源和能源发展战略角度,利用低品阶可再生能驱动CO₂转化合成化学品,将为CO₂资源化利用和可再生能转化并存储为化学能提供极大的发展空间,具有重大意义。目前,利用可再生能光电催化CO₂转化利用的研究方兴未艾,而人工生物转化CO₂作为重要的合成化学品新途径也受到越来越多的关注。通过模拟自然界中植物和微生物等的自然光合作用过程,设计和构建出人工光合体系,可使人工生物转化CO₂以更加高效的方式转化CO₂合成化学品。人工生物转化CO₂合成化学品是电催化、光催化和光电催化CO₂等过程的重要补充,主要包括微生物电合成、无机-生物杂化光合系统、PSII复合体系和代谢工程等关键技术。

微生物电合成(microbial electrosynthesis, MES)是在生物电化学系统中利用特定的微生物作为生物催化剂,以电能作为能量输入,通过生物反应将CO₂还原成多碳化合物的最有前途的新兴技术之一。用于MES的细菌和酶具备合成单一产物的功能,对于合成目标产物具有100%的选择性。以太阳能、风能等低品阶可再生电能作为其驱动能量,从而使MES成为一种更绿色和可持续的CO₂转换技术。MES中CO₂转化为高附加值化学品和生物燃料仍处于初步阶段,有许多技术和经济挑战需要解决,如低能量利用效率和CO₂转化率。

无机-生物杂化光合体系(photosynthetic biohybrid systems, PBS_s)是由细菌或酶固定在无机半导体光催化剂上组成的新型光驱动装置,将高效无机光催化剂与酶催化剂或细胞有机体结合起来,以接近或超过自然光合作用或单独化学催化的效率选择性地固定CO₂。PBS_s可在温和条件下以成本效益高的方式高选择性获得目标产物,并且具有合成大量长链碳分子的能力。该装置也可以理解为是MES反应器以太阳能为动力,或对MES电极进行改造,使其能够直接捕获光能,从而有效地成为一种比天然光合作用具有更高太阳能效率的人工光合作用装置。PBS_s目前还处于发展的初级阶段,虽然可以获得更

高的太阳能转换效率(10%–20%), 但进行实际应用仍有不少困难. 其中主要的挑战在于选择可兼容的光采集系统和高效的生物固碳元件, 以及生物和非生物组分的无缝集成, 即要克服跨生物和非生物界面上的电荷转移屏障.

PSII复合体系是最近提出来的一种由天然光合系统二(photosynthetic system II, PSII)和人工光催化剂组成的, 或用PSII对MES电极进行修饰, 辅助MES对CO₂还原的人工光化学体系. 与PBS_S相比, PSII复合体系的生物酶是PSII, 可以再现PSII的生物特征如优秀的光采集能力, PSII可以高效捕获可见太阳光光谱所有波长的能量, 并且有效地利用该能量驱动水分解产氢, 这也是无机光催化剂不具有的优势. 研究人员对利用PSII组装在电极上的光伏转换系统进行了大量研究, 并将其应用于CO₂光电化学合成, 目前已取得初步进展.

代谢工程(metabolic engineering)是根据细胞代谢网络对细胞代谢途径进行合理设计, 并利用分子生物学手段如重组DNA技术有目的地设计和调控生物体中已有的代谢网络和表达调控网络, 从而实现更高效的生物化学转化、能量转移以及积累目标产物的应用学科. 目前, 代谢工程被大量应用于光合生物固碳, 进一步优化CO₂到生物量或其他有机碳化合物的资源化利用. 通过对代谢工程的研究, 提高认识、设计和改造细胞代谢CO₂的能力, 从而获得低能耗、高效率的固碳途径, 推动生物固碳工业技术进步.

本文总结了近年来基于上述CO₂人工生物转化关键技术合成不同碳数化合物方面所取得的重要研究成果, 并对其未来发展趋势进行了展望.

关键词: 二氧化碳; 人工生物转化; 太阳能; 固碳; 化合物

收稿日期: 2019-03-23. 接受日期: 2019-05-11. 出版日期: 2019-10-05.

*通讯联系人. 电话: (021)20350954; 传真: (021)20350867; 电子信箱: chenw@sari.ac.cn

#通讯联系人. 电话: (021)20608005; 传真: (021)20350867; 电子信箱: weiwei@sari.ac.cn

基金来源: 国家自然科学基金(91745114, 21802160); 国家重点研发计划(2016YFA0202800); 中国科学院百人计划; 上海市扬帆计划(18YF1425700); 中国科学院上海高等研究院创新基金(Y756812ZZ1(172002), Y756803ZZ1(171003)).

本文的电子版全文由Elsevier出版社在ScienceDirect上出版(<http://www.sciencedirect.com/science/journal/18722067>).